



TRS value of sugarcane according to bioenergy and sugar levels

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ABSTRACT. In the specific case of sugarcane, producers in Brazil are currently paid by the content of total recoverable sugars (TRS) in the raw material when it reaches the industry, according to CONSECANA: $TRS = 9.6316 * PC + 9.15 * RSS$, where PC is the Pol in cane (apparent sucrose) and RSS are reducing sugars in sugarcane (glucose + fructose). The objective of the project was to propose changes in the procedures used to mathematically determine the TRS, estimating the calorific value of moist cake and weight of moist cake. The final model is then proposed: $TRS = 25.9892 + 0.02172 * CV_{mc} * WMC + 0.536 * WMC - 4.14 * CV_{mc} + 4.8158 * PC + 4.575 * RSS$. Thus we obtain the TRS calculated according to the calorific value of moist cake (CV_{mc}), weight of moist cake (WMC), Pol cane (PC) and the reducing sugars in sugarcane (RSS). This form is included in the estimation of TRS, the calorific value of moist cake, which reflects the bioenergy of fiber, weight of moist cake that estimates sugarcane fiber, in addition to existing factors Pol cane and reducing sugars in sugarcane. In the proposed model, the estimated values of TRS were 11.08% higher than the estimated values in the CONSECANA model.

Keywords: *Saccharum*, quality, biomass.

Valor de ATR da cana-de-açúcar em função de teores de bioenergia e açúcar

RESUMO. No caso particular da cana-de-açúcar, os produtores são remunerados atualmente no Brasil pelo teor de açúcares totais recuperáveis (ATR) que a matéria-prima apresenta ao chegar à indústria, segundo CONSECANA: $ATR = 9,6316 * PC + 9,15 * AR$, onde PC é a Pol da cana (sacarose aparente) e ARC são os açúcares redutores da cana (glicose + frutose). O objetivo do projeto foi propor alterações nos procedimentos utilizados para determinação matemática do ATR, estimando pelo poder calorífico do bolo úmido e peso do bolo úmido. O modelo final proposto fica então: $ATR = 25,9892 + 0,02172 * PC_{bu} * PBU + 0,536 * PBU - 4,14 * PC_{bu} + 4,8158 * PC + 4,575 * ARC$. Assim tem-se o ATR calculado em função do Poder calorífico do bolo úmido (PC_{bu}), peso do bolo úmido (PBU), Pol da cana (PC) e Açúcares Redutores da Cana (ARC). Desta forma inclui-se na estimativa dos valores de ATR o Poder calorífico do bolo úmido, que reflete a bioenergia da fibra, peso do bolo úmido que estima a fibra da cana, além dos fatores já existentes, Pol da cana e Açúcares Redutores da cana. O modelo proposto estimou valores de ATR 11,08% superiores que o modelo Consecana.

Palavras-chave: *Saccharum*, qualidade, biomassa.

Introduction

Biomass is an important energy source for the human race. It is the natural way of storing a fraction of incident solar energy in the planet, and even fossil fuels originated from biomass. The challenge facing humanity is to seek solutions for ever more efficient use of this natural resource (ROSSETO, 2012).

Analyzing the waste products from the most important commercial monocultures in the country, sugarcane stands out due to the abundance of straw residue (green leaves, dry leaves and tops) (SOUSA; MACEDO, 2010).

Historically, sugarcane has been harvested to obtain sugar, and more recently for ethanol production as well. In both cases, the interest is centered on maximizing production of sucrose and raw materials. A certain amount of fiber in the stem, which can vary between 10 and 15% in weight, was always able to meet the energy needs of a plant, even when operating rather inefficiently. Currently, special attention is being given to sugarcane fiber levels, as it is possible to use second-generation ethanol and lignin as energy sources in steam boilers. Under tropical conditions, some clones have been found to be able to accumulate more dry matter and higher levels of energy fiber (LEÓN

et al., 2010). And according to Inman-Bamber et al. (2011), some sugarcane clones can yield higher amounts of fiber without significant losses in sucrose levels, but possibly reducing total recoverable sugars (TRS), compromising quality-based payment. According to Rosseto (2012), a more efficient manner to compare plants according to quality of produced biomass is to convert all biomass into a single energy unit, which could be Joule (J); Mega Joule (MJ); Giga Joule (GJ) or ton of oil equivalent (1 toe = 42 GJ).

The bioelectricity generated from sugarcane bagasse has gained importance as a product in Brazilian power plants (MARTINES FILHO et al., 2006). In 2008, about 30 plants in Brazil negotiated an average of 544 MW for sale annually over 15 years. That volume generated US\$ 389.6 million in annual revenue (SOUSA; MACEDO, 2010).

With an increase of 4.3% over the previous harvest, sugarcane production in Brazil has expanded to an expected 8.5 million hectares in producing states for the 2012/13 season, with São Paulo state leading the pack with 4.42 million hectares. Total projections call for 596.63 million tons of sugarcane to be milled in the 2012/13 harvest, a 6.5% increase over the 2011/12 season, meaning that 36.3 million more tons will be milled than during the previous harvest (CONAB, 2012).

The essence of the current payment system (CONSECANA) is to reward sugarcane quality based on the prices of the final products obtained from this raw material; as such, there is no single price per ton, with variations according to climate factors, soil, variety, farming practices and marketing mix of the industrial unit. Soil tillage for crop placement can result in higher growth rates and lead to changes in quality at harvest time (TAVARES et al., 2010). Mechanized sugarcane harvest creates straw residue, which depending on the handling system can result in lower biomass and bioenergy production (CAMPOS et al., 2010). Revisions to the payment system are important to eliminate distortions and stimulate an improvement in the quality of raw materials (SACHS, 2007).

The research hypothesis was that the energy value of wet bagasse can create an additional parameter to calculate TRS in order to obtain a fair compensation for the material delivered at processing plants.

The objective of the project was to propose changes in the procedures used to mathematically determine TRS, estimated by the calorific value of moist cake and weight of moist cake, in addition to previously used factors – Calorific Value (CV), RSS

and Industrial Fiber. The intent is to collaborate towards a more accurate payment formula for sugarcane – one that does not necessarily imply higher prices, but rather values that better fit existing profit margins for the different by-products produced from the raw material.

Material and methods

A total of 128 sugarcane samples from the experiment were analyzed – 64 in 2010, and 64 in 2011. The soil in the experiments was characterized as a Dystrophic Red-Yellow Argisol, typical to moderate, with medium-clayish texture (SANTOS et al., 2006). The climate in the region is classified as Aw, with rainy summers and dry winters.

A DDS Cal2K bomb calorimeter was used to analyze the gross calorific value, in accordance with criteria set by the Brazilian Association for Technical Standards – ABNT in rule NBR 8693/84 (VALE et al., 2007). The analysis was carried out in moist cake obtained after milling (FERNANDES, 2003).

The Hawaiian method was used to analyze real fiber (VASECHI, 1968).

All data were charted and subjected to correlation analysis and graph creation using Microcal Origin 6.0 mathematical software.

Results and discussion

Considering the distribution of energy in sugarcane, the following model can be written:

$$\mathcal{E}_{sugarcane} = \mathcal{E}_{fiber} + \mathcal{E}_{sugars} + \mathcal{E}_{others\ organic\ materials} \quad (1)$$

In which:

$\mathcal{E}_{sugarcane}$ = Total energy in sugarcane

\mathcal{E}_{fiber} = energy of fiber in the sugarcane

\mathcal{E}_{sugars} = energy of sugars in the sugarcane

$\mathcal{E}_{other\ organic\ materials}$ = energy of non-sugars in the sugarcane

As the bioenergy of a material is determined by the gross calorific value, we get:

$$CV_{sugarcane} = \frac{F\%sugarcane}{100} * CV_{fiber} + \frac{TRS * CV_{sugar}}{90,5} + \frac{non - sugar\ organic * CV_{nso}}{100} \quad (2)$$

$CV_{sugarcane}$ = Calorific value of sugarcane

F%_{sugarcane} = Values of fiber in sugarcane in (%)

CV_{fiber} = Calorific value of sugarcane fiber

TRS = Total recoverable sugars (90.5% of all sugars in sugarcane)

CV_{nso} = Calorific value of non-sugar organic materials

As the level of non-sugar organic materials in sugarcane is 1.16%, TRS values are near 12% of sugarcane, and fiber averages 12%, non-organic materials represent 4.83% of the sum of TRS plus Fiber, making it possible to exclude it from the formula or leave it as a constant C:

$$CV_{sugarcane} = \frac{F\%sugarcane}{100} * CV_{fiber} + \frac{TRS * CV_{sugar}}{90,5} (+ C) \quad (3)$$

Isolating variable TRS, we get:

$$TRS = \left[CV_{sugarcane} - \frac{F\%sugarcane}{100} * CV_{fiber} (- C) \right] * \frac{90,5}{CV_{sugar}} \quad (4)$$

The Calorific value of sugar (CV_{sugar}) used was = 17 MJ kg⁻¹, the Calorific value of non-sugar organic materials (CV_{nso}) used was = 20 MJ kg⁻¹.

Using the data in Table 1, regressions were done using Origin 6.0 software.

Figure 1 presents the regression between the Calorific value of sugarcane obtained from analyses directly in the material and Calorific value of sugarcane calculated with the value of the Calorific value of moist cake obtained after pressing for analysis. Despite the low value of the coefficient of determination r^2 , it can be observed that the regression has a significant value at 1%. This denotes a strong correlation between the variables, indicating the possibility of calculating the Calorific value of sugarcane by performing analyses in the fibrous material (moist cake) produced by preparing the sample for payment purposes. In this case, as cited by Sachs (2007), revisions to the payment system can result in better quality sugarcane and stimulate producers; however, the COSECANA payment system is complex and quite structured, with the possibility of adding certain factors as long as they are mutually interesting for mill owners and sugarcane suppliers.

Table 1. Results obtained for variables Analyzed calorific value of sugarcane, Calculated calorific value of sugarcane, Real fiber, Fiber press method, Calorific value of real fiber, and Calorific value of moist cake.

(Figura 1)		(Figura 2)		(Figura 3)	
Calorific value of sugarcane Analyzed GJ kg ⁻¹	Calorific value of sugarcane Calculated with Moist cake GJ kg ⁻¹	Real fiber (%)	Fiber - Press Calculated	Calorific value Real fiber - analyzed (MJ kg ⁻¹)	Calorific value of moist cake (MJ kg ⁻¹)
3.25	2.30	9.71	11.48	18.08	8.69
3.70	3.03	10.65	11.35	18.09	11.57
3.75	2.79	11.23	11.19	17.46	10.80
4.77	2.04	9.62	10.74	21.19	8.27
5.09	2.69	10.24	11.53	18.39	10.10
4.10	3.07	10.32	12.21	27.45	10.82
4.49	2.62	10.07	11.24	17.69	10.12
4.76	2.53	10.43	11.01	20.33	10.00
3.88	3.62	11.09	10.66	18.01	14.80
5.77	2.91	11.44	13.51	18.74	9.21
6.00	3.45	11.26	14.13	16.21	10.42
.
7.65	2.69	9.62	12.26	18.16	9.46
5.27	2.44	11.32	13.37	18.40	7.82
6.34	2.27	13.02	12.20	18.12	8.03
6.47	2.93	11.70	13.40	16.42	9.36
7.90	3.18	12.26	12.78	21.75	10.69
4.64	2.69	11.68	12.31	18.24	9.42
5.86	3.36	11.20	12.60	20.28	11.48
5.35	1.91	12.24	10.77	18.12	7.72
4.86	2.68	11.66	11.98	18.51	9.66
5.14	3.39	13.72	13.31	18.70	10.90
8.08	2.72	12.26	13.27	25.80	8.79
6.47	3.14	12.06	14.11	18.32	9.48
5.56	3.18	10.68	13.21	18.57	10.30
5.10	3.36	11.04	14.06	26.60	10.18
8.72	3.83	11.88	13.53	18.81	12.11
5.49	2.82	11.58	12.56	17.09	9.64
6.19	3.68	14.22	13.95	20.67	11.26
8.46	3.25	13.00	14.35	18.40	9.64
5.61	2.45	11.52	12.32	18.71	8.57
6.12	2.93	9.72	13.16	14.94	9.54
5.85	2.77	13.18	13.04	18.64	9.11
5.58	2.99	9.82	12.95	17.15	9.91
7.40	4.27	11.62	12.79	18.17	14.33
6.73	2.97	11.24	13.17	18.60	9.67
5.53	2.76	11.18	12.09	26.73	9.83
5.87	3.70	10.82	13.07	17.52	12.14

The inclusion of the Calorific value of sugarcane should occur naturally, as Rosseto (2012) reports that the best way to compare plants is by their bioenergy, and their assessment to that end should be simple and without great changes in methodology.

Figure 2 presents the regression between real fiber analyzed directly in sugarcane and Industrial fiber calculated using the weight of moist cake (WMC). Despite the low value for the coefficient of determination r^2 , it can be seen that the regression has statistical value at 1%. This indicates a strong correlation between the variables. This consideration allowed CONSECANA to incorporate the calculation of Industrial fiber through WMC into the model already in place in Brazil.

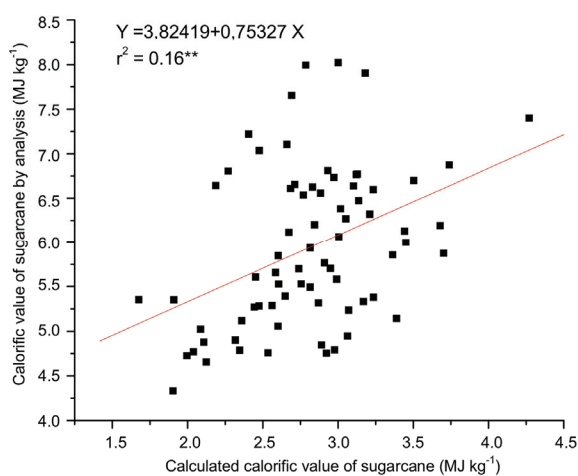


Figure 1. Mathematical regression model of the Calculated calorific value of sugarcane with WMC and the Calorific value of sugarcane by direct analysis.

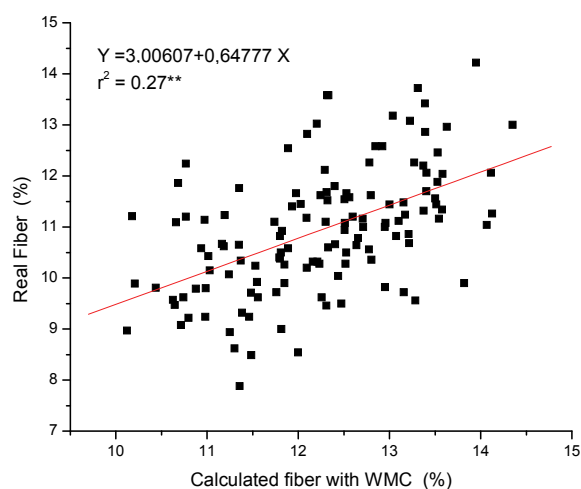


Figure 2. Mathematical regression model between Calculated fiber with WMC and Real fiber in sugarcane.

Figure 3 presents the regression between the Calorific value of real fiber analyzed directly in sugarcane fiber and the Calorific value of moist cake

(WB). It can be observed that the regression is statistically significant at 1%. This indicates a strong correlation between the variables.

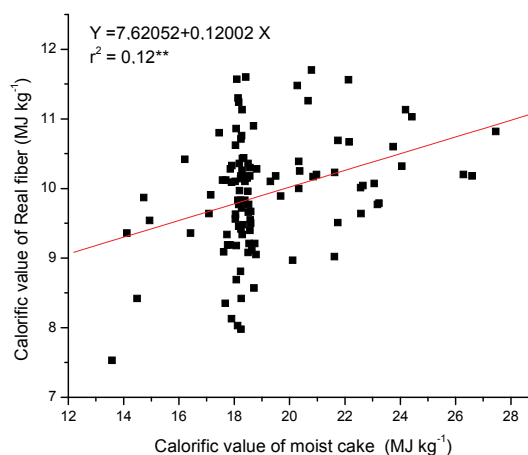


Figure 3. Mathematical regression model between Calorific value of moist cake and the Calorific value of Real fiber, determined in the material used to analytically determine real fiber.

In equation 4, the value of CV_{cane} (the first independent variable) can be calculated through the calorific value of moist cake, as shown in Figure 1; those data showed a correlation coefficient at 1%. The second independent variable shown in this model is $F\%_{\text{Cane}}$, which from Figure 2 can be calculated using the Weight of Moist cake (WMC), with a correlation coefficient at 1%, which is already used by the CONSECANA system. The third independent variable, CV_{fiber} , can be calculated from Figure 3 using the calorific value of moist cake. CV_{sugar} is constant, equal to 17 MJ kg⁻¹. Thus, the TRS value can be estimated by a mathematical model using the variables WMC and CVmc. As Figures 1, 2 and 3 show values for the regression coefficient of determination r^2 that are significant at 1%, it was decided to perform a multiple regression between TRS, Calorific value of sugarcane, calculated with the calorific value of moist cake, Fiber calculated with the weight of moist cake and calorific value of moist cake.

The following model is obtained (Table 2), adjusted to the values:

$$Y = 40.24 + 21.72 \cdot X1 + 13.4 \cdot X2 - 8.28 \cdot X3 \quad (5)$$

in which:

Y = Total recoverable sugars, estimated; $X1$ = Calorific value of sugarcane calculated with the calorific value of moist cake; $X2$ = Fiber calculated with the moist cake obtained during pressing; $X3$ = Calorific value of moist cake; $R^2 = 0.60^{**}$; $CV = 9.17\%$ between calculated TRS values and real TRS values.

Table 2. Values of r, F-test and Coefficients of the multiple regression model between TRS (Y), Calorific value of sugarcane, calculated with the calorific value of moist cake (X1), Fiber calculated with the moist cake obtained in pressing (X2) and calorific value of moist cake (X3).

Regression statistic					
R-multiple					0.773747483
R-squared					0.598685168
Adjusted R-squared					0.581236697
Standard error					8.650817496
Observation					73

ANOVA					
	Gl	SQ	QM	F	significance
Regression	3	7703.30	2567.77	34.31	1.09E-13
Waste material	69	5163.73	74.84		
Total	72	12867.03			

	Coefficients	Standard error	t-stat	P-value	Bottom 95%
Intersection	40.24	71.62	0.28	0.78	-122.75
Variable X 1	21.72	23.92	0.45	0.65	-36.86
Variable X 2	13.4	6.16	1.09	0.28	-5.59
Variable X 3	-8.28	6.42	-0.65	0.52	-16.95

It has also (CONSECANA, 2011):

$$F_{\text{industrial}} = 0.08 \cdot \text{WMC} + 0.876 \quad (12)$$

$$Y = 9.6316 \cdot X_4 + 9.15 \cdot X_5 \quad (6)$$

The final model is therefore:

- In which:
- X4 = Pol in Cane (PC);
- X5 = Reducing sugars in sugarcane (RSS).

$$\begin{aligned} \text{TRS} = & 20.12 + 10.86 \cdot \left(\frac{\text{CVmc}}{500}\right) \cdot \text{WMC} + \\ & 6.70 \cdot (0.08 \cdot \text{WMC} + 0.876) - 4.14 \cdot \text{CVmc} + \\ & 4.8158 \cdot \text{PC} + 4.575 \cdot \text{RSS} \end{aligned} \quad (13)$$

By adding equations 5 and 6, we get:

$$Y = 40.24 + 21.72 \cdot X_1 + 13.4 \cdot X_2 - 8.28 \cdot X_3 \quad (5)$$

We therefore obtain TRS calculated as a function of the Calorific value of moist cake (CVmc), weight of moist cake (WMC), Pol in sugarCane (PC) and Reducing Sugars in Sugarcane (RSS), equations 14.

$$Y = 9.6316 \cdot X_4 + 9.15 \cdot X_5 \quad (6)$$

$$2Y = 40.24 + 21.72 \cdot X_1 + 13.4 \cdot X_2 - 8.28 \cdot X_3 + 9.6316 \cdot X_4 + 9.15 \cdot X_5 \quad (7)$$

$$Y = \frac{40.24 + 21.72 \cdot X_1 + 13.4 \cdot X_2 - 8.28 \cdot X_3 + 9.6316 \cdot X_4 + 9.15 \cdot X_5}{2} \quad (8)$$

$$\begin{aligned} \text{TRS} = & 25.9892 + 0.02172 \cdot \text{CVmc} \cdot \\ & \text{WMC} + 0.536 \cdot \text{WMC} - 4.14 \cdot \text{CVmc} + \\ & 4.8158 \cdot \text{PC} + 4.575 \cdot \text{RSS} \end{aligned} \quad (14)$$

$$Y = 20.12 + 10.86 \cdot X_1 + 6.70 \cdot X_2 - 4.14 \cdot X_3 + 4.8158 \cdot X_4 + 4.575 \cdot X_5 \quad (9)$$

or,

$$\begin{aligned} \text{TRS} = & 20.12 + 10.86 \cdot \text{PCCCCVMC} \\ & + 6.70 \cdot \text{Fpmc} - 4.14 \cdot \text{CVmc} + 4.8158 \cdot \text{PC} \\ & + 4.575 \cdot \text{RSS} \end{aligned} \quad (10)$$

The press methodology used 500 g of shredded sugarcane; WMC is obtained after pressing, ranging from 110 to 160 g. In order to transform the calorific value of WMC into the calorific value of sugarcane, the following model should be used:

$$\text{PCCCCVMC} = \left(\frac{\text{CVmc}}{500}\right) \cdot \text{WMC} \quad (11)$$

In the CONSECANA methodology, the industrial fiber calculated with WMC follows the model below:

Table 3 shows that of the 128 analyses undertaken, the proposed model estimated TRS, on average, to be 1.25 kg more per ton of sugarcane than the traditional CONSECANA formula, which obtained an average of 88.96. However, the model estimated both higher and lower values than the CONSECANA model, depending on the percentage composition of the components in the model. Therefore, the proposed formula estimated values with 11.08% more TRS; this may be related to the C constant obtained from the calorific value of non-sugar organic materials, for which there are no routine analyses in raw-material sugarcane for payment purposes.

Table 3. TRS values calculated with the original CONSECANA model, confronted against the proposed model, which takes into account the calorific value of moist cake and the amount of moist cake produced in 0.5kg of pressed sugarcane.

TRS	TRSprposed	dev.	dev. ²	PC	RSS	PCCCCVMC	Fpmc	CVmc
123.53	147.85	24.32	591.42	12.08	0.79	2.30	11.48	08.69
130.23	146.28	16.05	257.51	12.73	0.83	3.03	11.35	11.57
119.18	140.23	21.06	443.32	11.57	0.84	2.79	11.19	10.80
138.17	149.07	10.90	118.89	13.68	0.70	2.04	10.74	08.27
136.48	153.00	16.52	272.95	13.47	0.74	2.69	11.53	10.10
140.21	160.52	20.31	412.48	13.92	0.67	3.07	12.21	10.82
143.35	153.68	10.32	106.56	14.20	0.72	2.62	11.24	10.12
143.39	151.73	08.35	069.71	14.24	0.68	2.53	11.01	10.00
124.76	131.96	07.20	051.90	12.19	0.81	3.62	10.66	14.80
126.24	135.15	08.90	079.29	12.45	0.69	2.35	10.18	10.09
120.60	139.04	18.44	339.97	11.72	0.84	2.05	10.63	08.42
118.95	130.28	11.33	128.34	11.56	0.83	3.53	10.71	14.35
110.59	134.19	23.60	556.95	10.62	0.90	2.59	10.93	10.28
103.07	122.34	19.28	371.64	9.80	0.95	3.38	10.64	13.86
115.07	130.49	15.41	237.56	11.10	0.89	2.12	10.12	09.19
115.60	142.53	26.92	724.82	11.24	0.81	2.11	11.25	08.13
124.89	144.08	19.18	368.05	12.16	0.85	2.00	10.88	07.98
142.62	162.43	19.81	392.43	14.19	0.65	2.74	12.16	09.72
125.84	144.21	18.37	337.36	12.93	0.15	2.60	11.16	10.12
119.53	142.84	23.31	543.58	11.57	0.89	3.09	11.55	11.60
113.63	131.62	17.99	323.56	11.06	0.78	2.36	10.44	09.87
..
140.58	157.00	16.42	269.71	16.32	0.00	2.90	11.80	10.62
147.73	161.78	14.04	197.23	15.34	0.00	2.67	11.82	09.77
150.38	167.97	17.59	309.31	14.92	0.73	2.68	12.30	09.40
136.13	152.46	16.33	266.82	13.12	1.07	1.68	10.98	06.64
140.81	149.31	08.50	072.33	14.47	0.16	2.27	10.77	09.18
146.01	159.74	13.73	188.57	14.63	0.55	3.23	11.93	11.70
136.75	155.96	19.21	368.91	13.38	0.86	2.60	11.76	09.56
149.50	166.79	17.29	298.81	14.75	0.81	2.93	12.32	10.25
145.75	175.19	29.45	867.05	14.35	0.82	3.24	13.41	10.33
159.85	162.66	02.81	007.92	16.20	0.42	2.71	11.35	10.36
152.04	163.20	11.16	124.57	15.08	0.74	2.77	11.79	10.15
152.67	164.34	11.67	136.18	16.34	0.00	2.82	11.89	10.23
154.72	171.15	16.43	270.02	15.65	0.44	3.00	12.51	10.32
138.41	160.52	22.11	488.87	13.77	0.63	2.89	12.23	10.18
151.49	174.51	23.02	529.92	15.10	0.66	3.02	13.00	09.96
162.85	185.24	22.39	501.32	16.43	0.50	3.18	13.54	10.04
159.70	175.45	15.75	248.14	16.10	0.51	2.46	12.51	08.46
171.75	176.18	04.44	019.67	17.36	0.50	2.77	12.09	09.89
178.67	184.21	05.53	030.63	18.11	0.47	2.69	12.51	09.25
149.37	172.35	22.98	528.20	15.01	0.52	3.13	12.92	10.39
179.49	182.83	03.34	011.13	18.16	0.50	2.67	12.33	9.34
179.64	186.08	06.44	041.52	18.14	0.54	3.18	12.80	10.67
172.16	178.92	06.76	045.74	17.39	0.51	3.06	12.44	10.60
150.66	206.94	56.28	3167.42	15.11	0.56	2.62	12.40	09.40
averages								
140.30	156.47							
VC =	11.08%							

Conclusion

It is possible to estimate TRS values using the Calorific value of moist cake, weight of moist cake, Pol in cane and Reducing Sugars in sugarcane.

The proposed model estimated TRS values to be 11.08% higher than in the CONSECANA model, due to non-sugar organic materials.

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